

# METROLOGY *for* HYDROGEN VEHICLES

## Design of gravimetric primary standards for field testing of hydrogen refuelling stations

*Marc de Huu, Martin Tschannen, Hugo Bissig (METAS)  
on behalf on the MetroHyVe project partners*

FLOMEKO 2019, Lisbon  
26-28 June 2019

# EMPIR Metrology for Hydrogen Vehicles



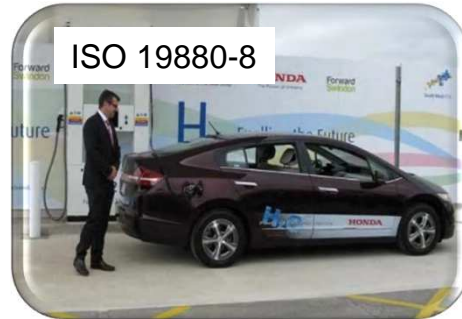
OIML R139-1

WP1: Flow metering



ISO 14687-2

WP2: Quality assurance



ISO 19880-8

WP3: Quality control

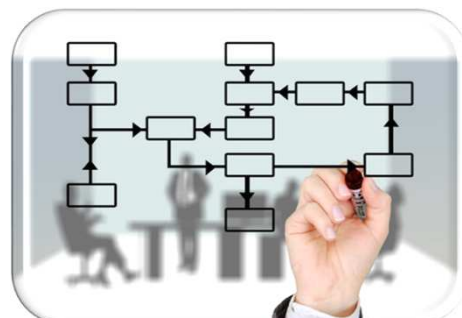


ISO 19880-1

WP4: Sampling



WP5: Creating impact



WP6: Management

20 project partners:

June 2017 – May 2020

Project co-ordinator:  
 Arul Murugan

## Other talks from MetroHyVe



Who	When	Where	Title
Oliver Bucker	Wed 11:30 to 13:00	Session S2.9, room 5	Pressure dependence of Coriolis mass flow meters used at hydrogen refuelling stations
Remy Maury	Thu 11:30 to 13:00	Session S10.5, room 2	Hydrogen refuelling station calibration with a traceable gravimetric standard
Marc MacDonald	Fri 11:30 to 13:10	Session S19.9, room 2	Air and Nitrogen testing of Coriolis flow meters designed for hydrogen refuelling stations

# Introduction



Aim of this project:

- Development of a metrological infrastructure for hydrogen vehicles because hydrogen fueling is critical to the success of a hydrogen economy



all stations  in operation  planned  old projects © Copyright Ludwig-Böllkow-Systemtechnik



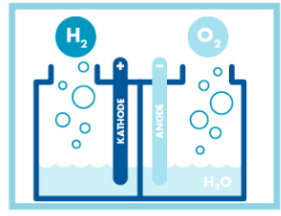
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# Introduction



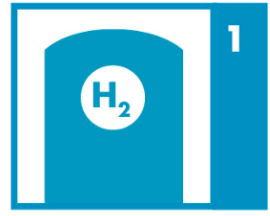
Shell Hydrogen Study © Shell

UPSTREAM

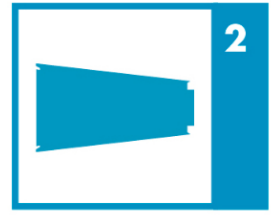


Electrolyser

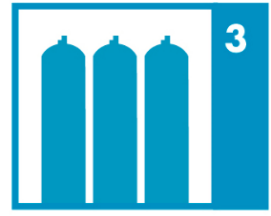
REFUELLING STATION



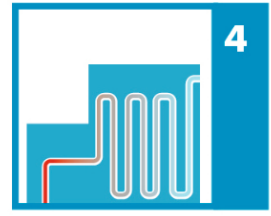
1 Low-Pressure Storage



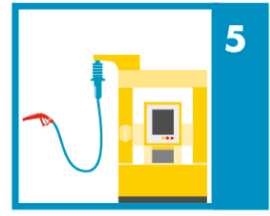
2 Compressor



3 High-Pressure Storage



4 Precooling

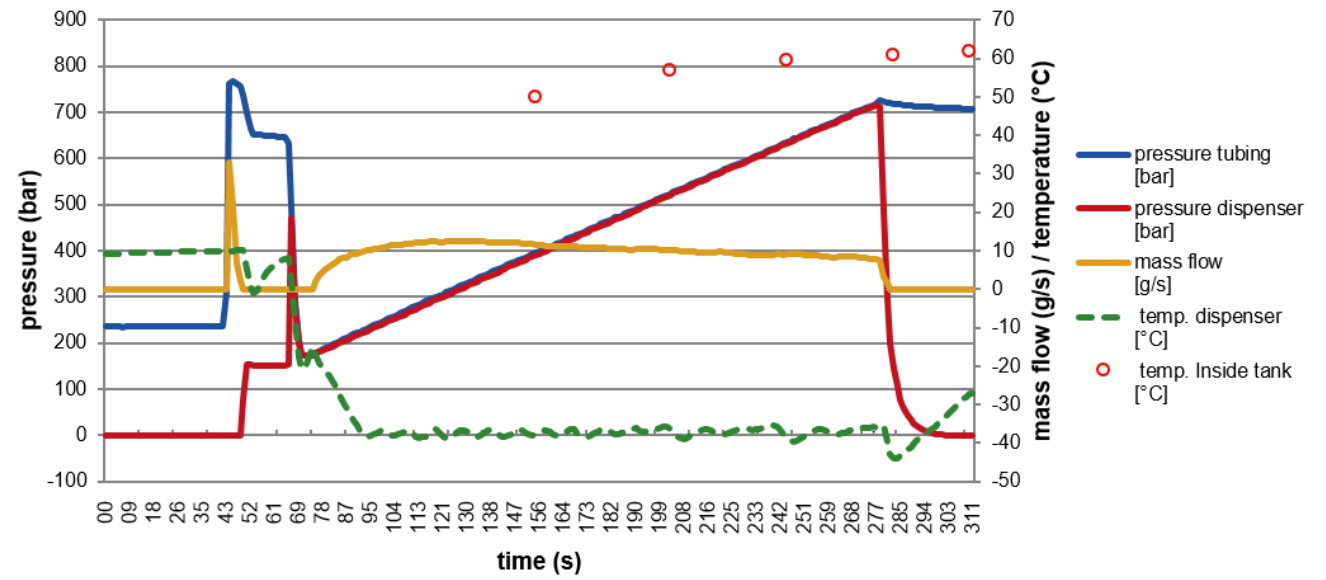


5 Dispenser



J2601<sup>®</sup>

(R) Fueling Protocols for Light Duty Gaseous Hydrogen Surface Vehicles





# Introduction

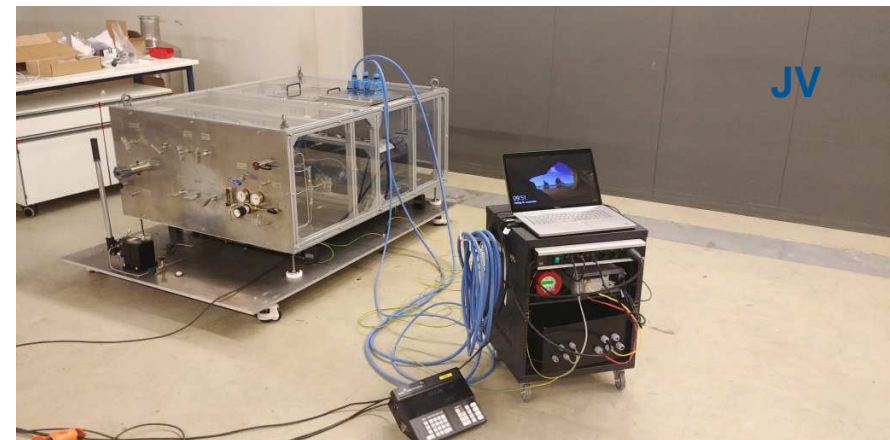
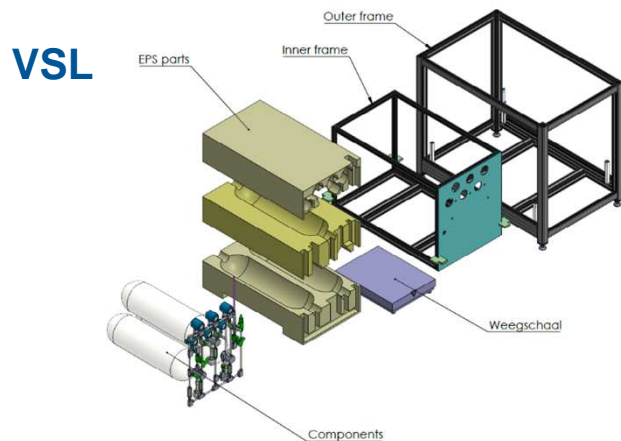


OIML R139-1  
International Recommendation  
Compressed gaseous fuel measuring systems for vehicles  
Part 1: Metrological and technical requirements

Table 1 - MPE values

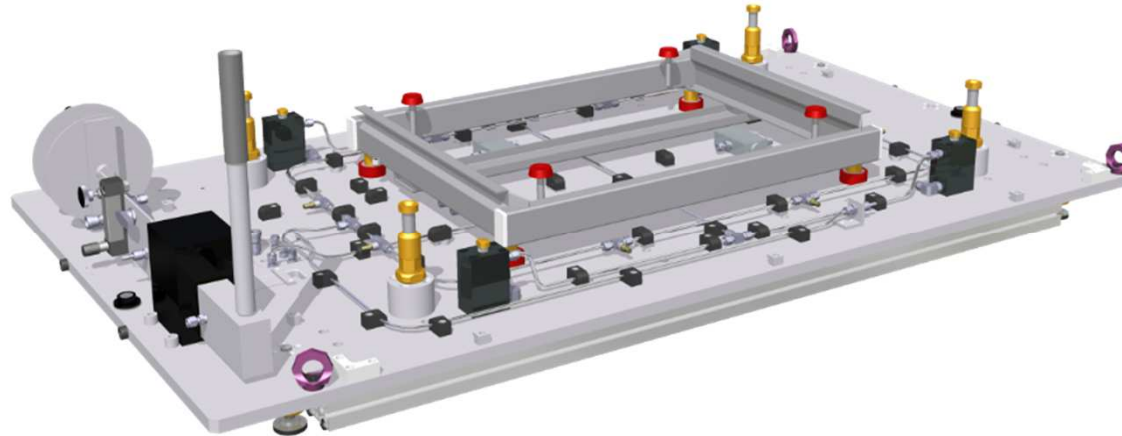
Accuracy class	MPE for the meter [in % of the measured quantity value]	MPE for the complete measuring system [in % of the measured quantity value]	
		at type evaluation, initial or subsequent verification	in-service inspection under rated operating conditions
For general application	1.5	1	2
For hydrogen only	2	1.5	3
	4	2	5

Develop mobile gravimetric standard for field testing with 1/5 of MPE (0.3%)



# Design of METAS field test standard

METAS Hydrogen Field Test Standard (HFTS)



# Design of METAS field test standard





# Design of METAS field test standard



36 L type 4 cylinders  
1.44 kg H<sub>2</sub> @ 70 MPa

Pt 100 probe, 27 cm  
inserted in tank

100 MPa pressure transducer

Venting line

300 kg scale  
0.1 g resolution

Medium pressure ¼" tubing, NPT  
and FK series fittings and valves  
in 316-stainless steel



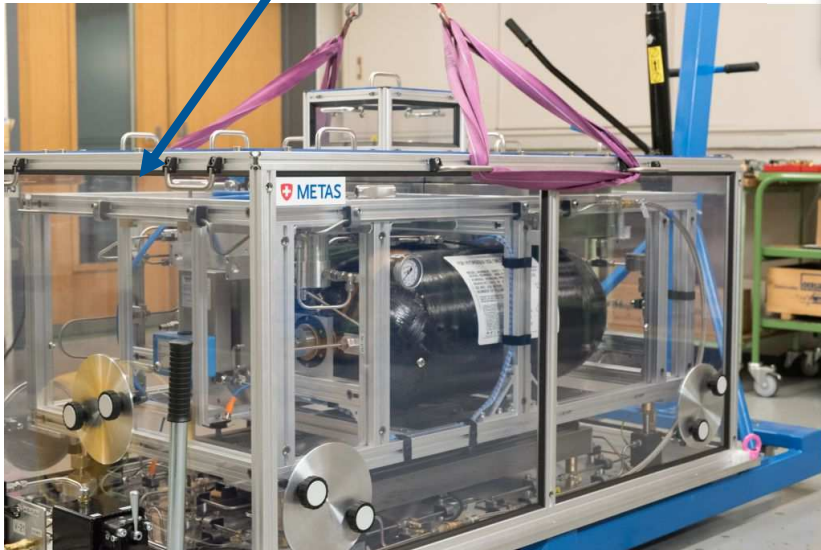
# Design of METAS field test standard



ESD plastic frame to protect the scale from the environment, acts like a greenhouse

Environment with explosive atmosphere → **certification**

ESD Plastic frame can be moved for better air circulation



Federal Institute of Metrology METAS  
Lindenweg 50, 3003 Bern-Wabern

Model: Hydrogen Field Test Standard (HFTS)  
Ident. No.: MM008831, Version 1.0  
Manufactured: 2018

**Ex II 3G Ex h IIC T4 Gc**  
SEV 18 ATEX 0110



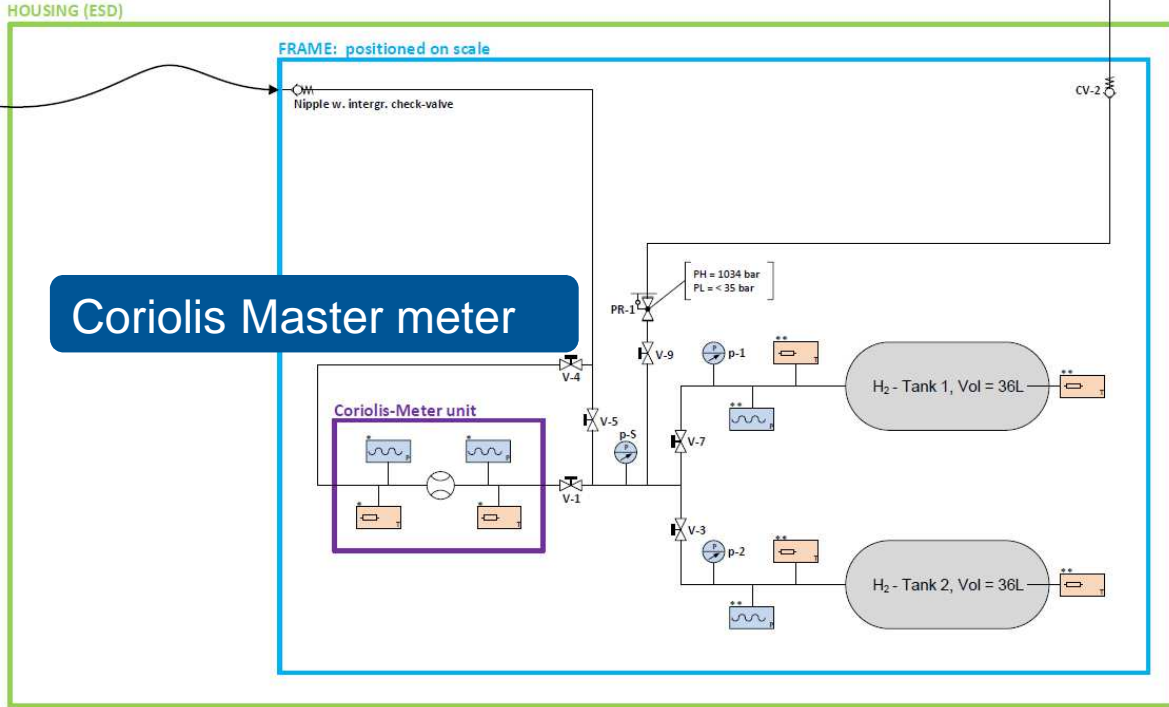
# Design of METAS field test standard



Inlet line connected to hydrogen dispenser

Venting line

- (Coriolismeter)
- Transmitter
- Pressure indication (Manometer)
- Thermometer (PT100)
- Needle valve
- Check valve
- Pressure reducing valve
- \* Optional
- \*\* Ready for read-out



Coriolis Master meter

# Design of METAS field test standard



Inlet line connected to hydrogen dispenser

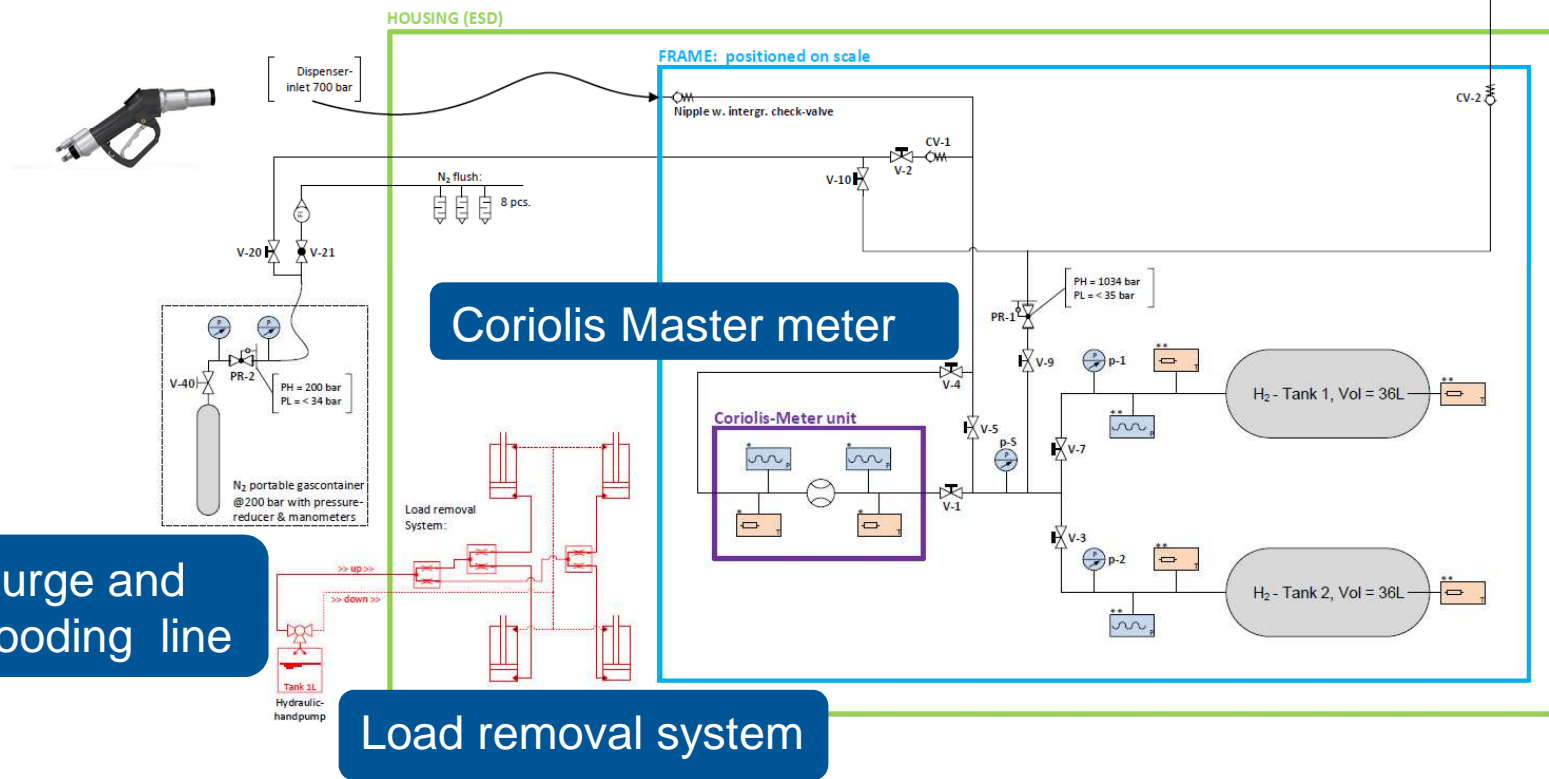
Venting line

Coriolis Master meter

Purge and flooding line

Load removal system

- Rotameter (Rotameter)
- Coriolis meter (Coriolismeter)
- Transmitter
- Pressure indication (Manometer)
- Thermometer (PT100)
- Ball valve
- Needle valve
- Shut-Off valve
- Check valve
- Pressure reducing valve
- Diffuser
- Actuator
- Flow divider
- \* Optional
- \*\* Ready for read-out





# Measurement method

Mass after and before fill

$$m_{H_2} = m_2 - m_1$$

Thermal expansion  
... negligible

pressure expansion  
0.92 L @ 70 MPa

$$V_{tank} = V_0 \cdot (1 + 3 \cdot \alpha \cdot \Delta T) \cdot (1 + \lambda \cdot \Delta P)$$

Scale readings

$$m_{H_2} = (W_2 - W_1) \cdot \left(1 - \frac{\rho_0}{\rho_N}\right) + V_0 \cdot [\rho_{air2} \cdot (1 + \lambda \Delta P_2) - \rho_{air1} \cdot (1 + \lambda \Delta P_1)] + V_{frame} \cdot (\rho_{air2} - \rho_{air1})$$

Buoyancy correction

Weigh empty tank

- **before:** disconnect all cables and hoses from the frame and lower the HFTS on the scale
- **after:** Lift the HFTS and connect all cables and hoses

Fill the tanks

- **before:** connect gas source
- **during:** monitor and record data
- **after:** disconnect gas source

Weigh full tank

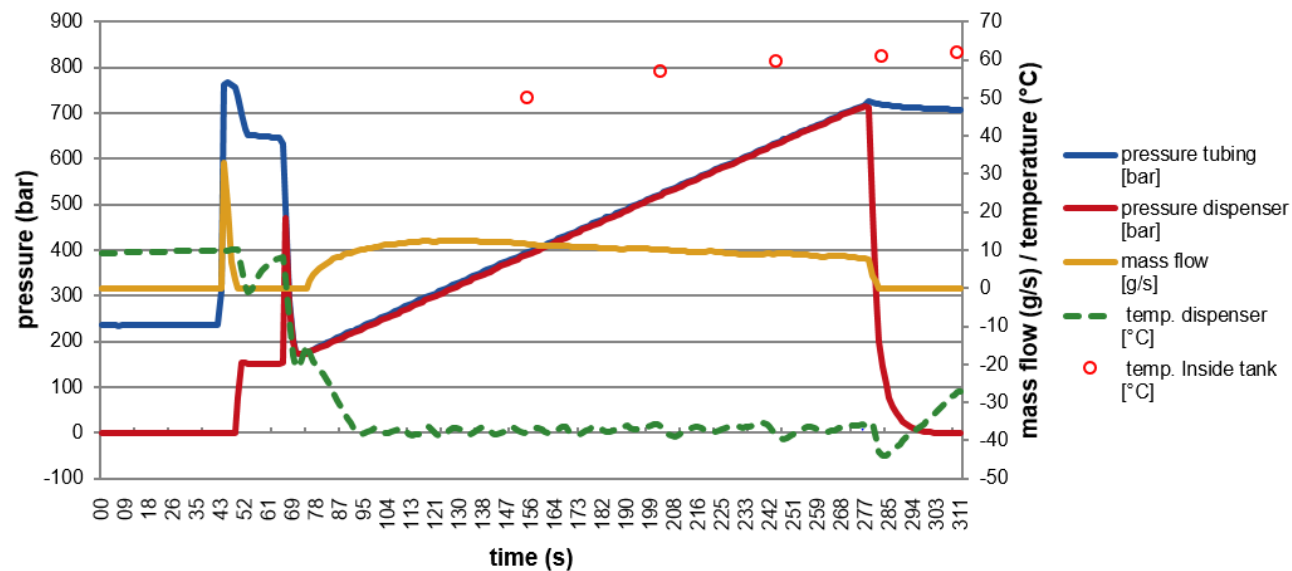
- **before:** disconnect all cables and hoses from the frame and lower the HFTS on the scale
- **during:** wait until scale reading stabilises and record value
- **after:** Lift the HFTS from the scale, connect all sensors and connect the vent stack to blow down the gas



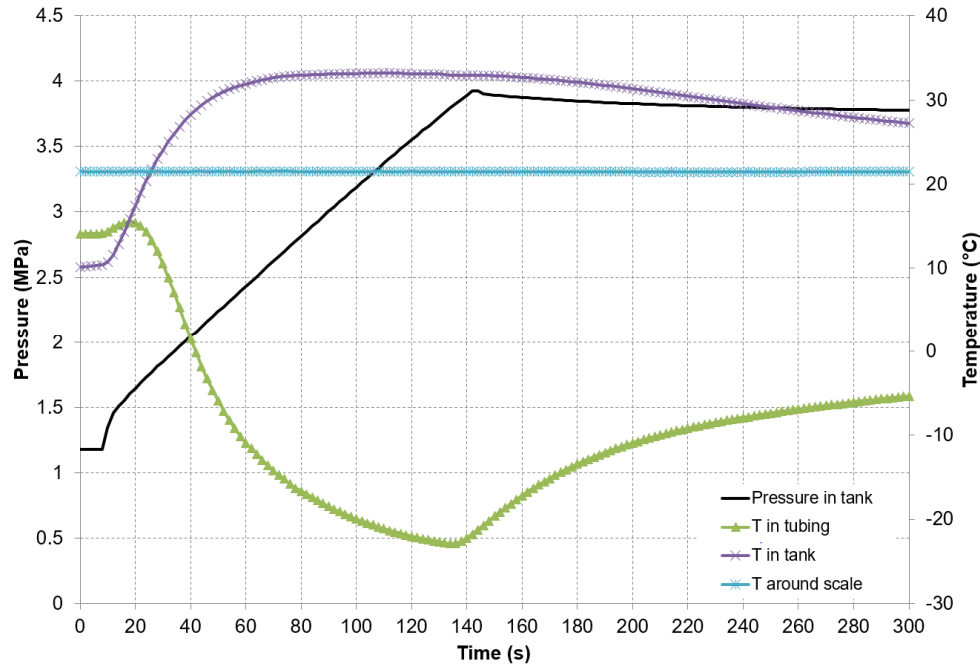
# Laboratory tests with N<sub>2</sub> @ -40°C



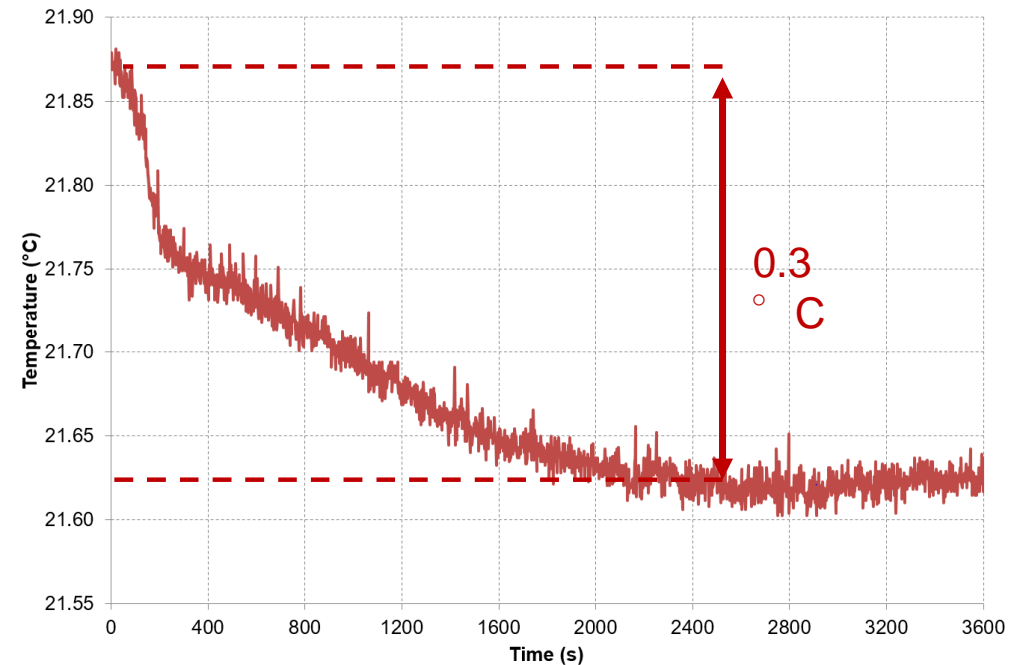
- Reproduce field tests as closely as possible and elaborate a testing procedure
- 5.5 MPa N<sub>2</sub> source, cooled down to -40°C to reproduce temperature conditions of hydrogen delivered by a HRS



# Laboratory tests with N<sub>2</sub> @ -40°C

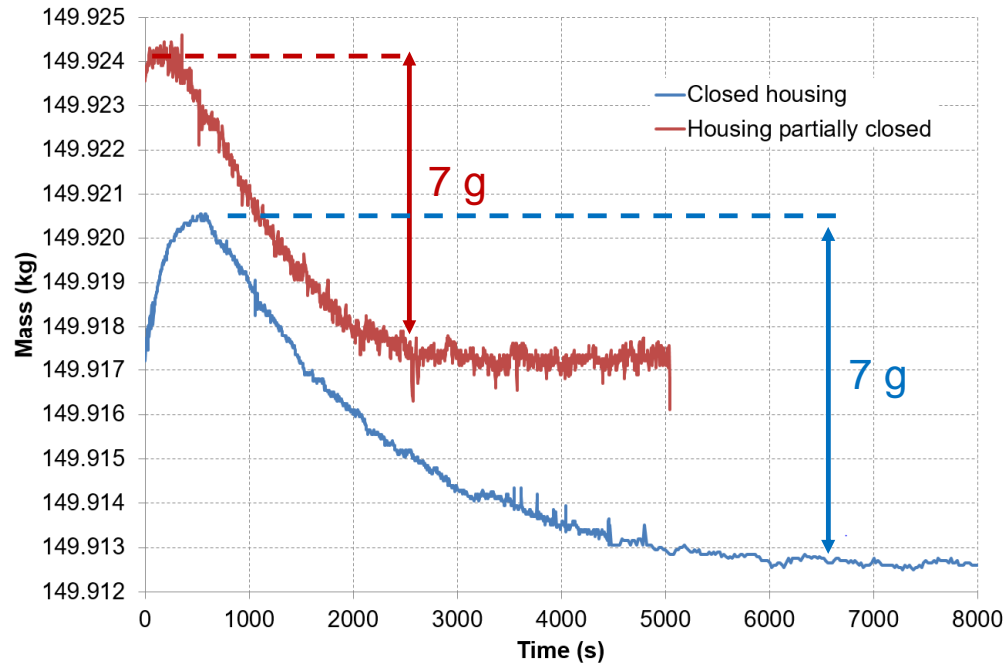


- Temperature increase in tank due to compression heating
- Tubing temperature below freezing point of water during fill
- Temperature around scale is constant

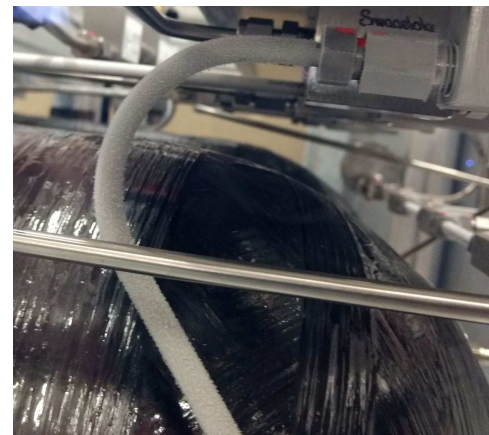


- Temperature profile around scale after fill with a closed housing
- Heat transfer from tank to air

# Laboratory tests with N<sub>2</sub> @ -40°C



- Cold gas freezes humidity on pipes
- Ice is not part of mass of dispensed gas
- Scale reading profile after fill shows melting and evaporation of ice
- Better air circulation accelerates loss of mass



# Uncertainty budget



Uncertainty component	Nominal value	$u(x_i)$ %	Contribution %
Initial mass	150.0000 kg	$4.7 \cdot 10^{-4}$	40.5
Final mass	151.0000 kg	$4.7 \cdot 10^{-4}$	40.5
Tank volume	0.120 m <sup>3</sup>	4.17	0.16
Frame volume	0.070 m <sup>3</sup>	7.14	< 0.1
Initial air density	1.1500 kg/m <sup>3</sup>	0.15	8.9
Final air density	1.1500 kg/m <sup>3</sup>	0.15	9.0
Initial tank pressure	0.10 MPa	20	< 0.1
Final tank pressure	35.00 MPa	0.057	< 0.1
Pressure coefficient	$2.2 \cdot 10^{-10}$ Pa <sup>-1</sup>	10	0.93

- Expanded uncertainty for the gravimetric method: 0.22 %
- Contribution from icing and condensation can be minimised if we wait long enough: 1 g spread (k=1)
- Expanded uncertainty for measurements in the field: 2.5 g for 1 kg (0.25%)
- Required uncertainty of 0.30% is achieved
- Measurements in the field under real conditions to validate some assumptions



# Summary



- Presented design of METAS HFTS
- Presented experimental results with HFTS under laboratory conditions with  $N_2$  gas at  $-40^\circ C$  to mimic real fill conditions
- Varying temperature and scale reading profiles
- Condensation on pipes leads to change of mass over time  $\rightarrow$  not negligible
- Presented uncertainty budget:  $U = 0.25\%$
- Guide for future designs of similar field testing instruments based on gravimetric principle







THANK YOU



**Marc de Huu**

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